

CLAIMS:

*Sub A1*  
5  
1. A late transition metal catalyst system comprising a Group 9, 10 or 11 metal complex stabilized by a bidentate ligand structure immobilized on a solid support where the catalyst loading is less than 100 micromoles transition metal compound per gram of solid support.

*Sub A2*  
10 2. The catalyst system of claim 1 wherein said *solid* particle support comprises silica.

*Sub A2*  
15 3. The catalyst system of claim 1 wherein the supported catalyst is a homogeneous supported catalyst.

15 4. The catalyst system of claim 1 wherein the metal complex is a first row metal complex.

*Sub A3*  
20 5. The catalyst system of claim 1 comprising a Group 9, 10 or 11 metal complex stabilized by a bidentate ligand structure having conjugated groups on a bridging element in said ligand.

25 6. A late transition metal catalyst system comprising a Group 9, 10 or 11 metal complex stabilized by a bidentate ligand structure, an organoaluminum compound, and a solid support.

25 7. The catalyst system of claim 6 wherein the organoaluminum compound is an alumoxane.

*system*  
A 8. The catalyst of claim 7 wherein the metal complex to alumoxane molar ratio is from about 1:500 to 10:1.

30 9. The catalyst system of claim 6 wherein the Group 9, 10 or 11 metal complex is represented by the formula:

$LMX_r$

35 wherein L is a bidentate ligand that stabilizes a square planar geometry and charge balances the oxidation state of  $MX_r$ ; X is independently selected from the group consisting of a halogen, alkoxide, aryloxide, amide, phosphide or other univalent anionic ligand, or two such X are joined to form an anionic chelating ligand;

and r is 0, 1, 2 or 3.

10. The catalyst system of claim 6 wherein said ~~particle~~ support comprises silica.

*solid*

5 Sub 11. The catalyst system of claim 6 wherein the supported catalyst is a homogeneous supported catalyst.

10 Sub 12. The catalyst system of claim 6 wherein the metal complex is a first row metal complex.

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13. A late transition metal catalyst system essentially without residual solvent comprising a Group 9, 10 or 11 metal complex stabilized by a bidentate ligand structure immobilized on a solid support.

*Sub A5*

*Solid*

15 14. The catalyst system of claim 13 wherein said ~~particle~~ support comprises silica.

*Sub A6*

15. The catalyst system of claim 13 wherein the supported catalyst is a homogeneous supported catalyst.

20 16. The catalyst system of claim 13 wherein the metal complex is a first row metal complex.

17. The catalyst system of claim 13 wherein said complex is an ionic catalyst comprising a metal cation and a noncoordinating anion.

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18. The catalyst system of claim 17 wherein the noncoordinating anion is *tetrakis(perfluorophenyl)borate*

30 19. The catalyst system of claim 17 wherein the ionic catalyst is prepared using an anion ionizing precursor that is a halide salt of Group 13-16 metals or metalloids.

Sub 20. 20. The catalyst of claim 17 wherein the metal complex to ionizing anion precursor molar ratio is from about 10:1 to 1:10.

35 21. The catalyst system of claim 1 wherein said complex is an ionic catalyst comprising a metal cation and a noncoordinating anion.

22. The polymerization process for polymerizing olefinically unsaturated monomers comprising contacting one or more of ethylene, C<sub>3</sub>-C<sub>20</sub> olefin, C<sub>4</sub>-C<sub>20</sub> cyclic olefin, C<sub>4</sub>-C<sub>20</sub> non-conjugated diolefin, C<sub>8</sub>-C<sub>20</sub> aromatic substituted olefin, C<sub>4</sub>-C<sub>20</sub> gem-substituted olefins, or C<sub>20</sub>-C<sub>1000</sub> olefin macromer with the catalyst system of claim 1.

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23. The polymerization process of claim 22 comprising conducting said contacting under gas phase polymerization conditions.

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24. The polymerization process of claim 23 wherein the reactor temperature is from -100 °C to 150 °C and at a pressure up to 7000 kPa.

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25. The polymerization process of claim 24 additionally comprising a scavenging compound.

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26. The polymerization process of claim 22 comprising conducting said contacting under slurry polymerization conditions.

27. The polymerization process of claim 26 wherein the reactor temperature is from 0 °C to 150 °C and at a pressure from 0.76 MPa to 4.8 Mpa

28. The polymerization process for polymerizing olefinically unsaturated monomers comprising contacting one or more of ethylene, C<sub>3</sub>-C<sub>20</sub> olefin, C<sub>4</sub>-C<sub>20</sub> cyclic olefin, C<sub>4</sub>-C<sub>20</sub> non-conjugated diolefin, C<sub>8</sub>-C<sub>20</sub> aromatic substituted olefin, C<sub>4</sub>-C<sub>20</sub> gem-substituted olefins, or C<sub>20</sub>-C<sub>1000</sub> olefin macromer with the catalyst system of claim 6.

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29. The polymerization process for polymerizing olefinically unsaturated monomers comprising contacting one or more of ethylene, C<sub>3</sub>-C<sub>20</sub> olefin, C<sub>4</sub>-C<sub>20</sub> cyclic olefin, C<sub>4</sub>-C<sub>20</sub> non-conjugated diolefin, C<sub>8</sub>-C<sub>20</sub> aromatic substituted olefin, C<sub>4</sub>-C<sub>20</sub> gem-substituted olefins, or C<sub>20</sub>-C<sub>1000</sub> olefin macromer with the catalyst system of claim 13.

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add A8

add  
H6